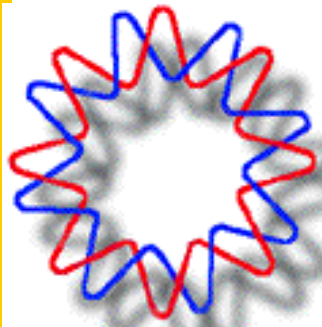




Biorrefinerías

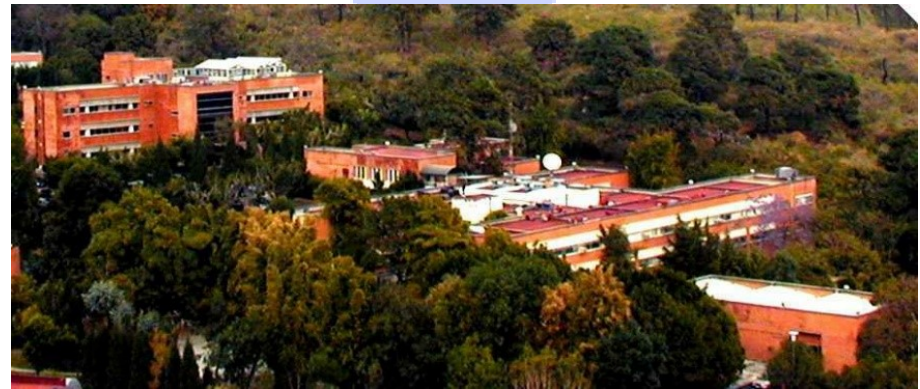
Aprovechamiento de biomasa vegetal usando microorganismos como biofabricas



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Instituto de Biotecnología - UNAM



Campus Morelos
www.ibt.unam.mx
Cuernavaca



IICA. CoMABio. SADER.
CONVERSATORIO SOBRE BIOECONOMÍA: UNA PERSPECTIVA DE
AGRICULTURA SUSTENTABLE Y GIRA TECNOLÓGICA.
Cuernavaca, Mor. 22/Ago/2019



Ingeniería Metabólica y Biología Sintética de Microorganismos



- ❑ Ingeniería metabólica y de bioprocesos, biología sintética y evolución adaptativa de *Escherichia coli* (a partir de 2018 con *Saccharomyces cerevisiae*), para la obtención de productos que sustituyan derivados del petróleo: biocombustibles (etanol carburante, alcoholes de cadena larga, 2,3 butanodiol) y precursores de biopolímeros biodegradables (D y L – lactatos, piruvato, butirato, succinato, R-3-HB).
- ❑ Estudios fisiológicos para la producción de biomasa con microalgas oleaginosas.



Global Challenge: New fuels & materials are needed to substitute fossil fuels and oil derivatives



Oil

- ✓ Depletion (Mexico)
- ✓ Price Variability
- ✓ Contamination-Spills
- ✓ Emissions
- ✓ Economic National Support

CO₂ Accumulation
Climatic Change
Global Warming



Oil, natural gas and carbon:
 Industrial activities, electricity
 generation, transport, etc.

Non-biodegradable
 Product accumulation



Alternative E

Wind
Hydro
Waves
Geothermic
Nuclear
Solar:

Electricity

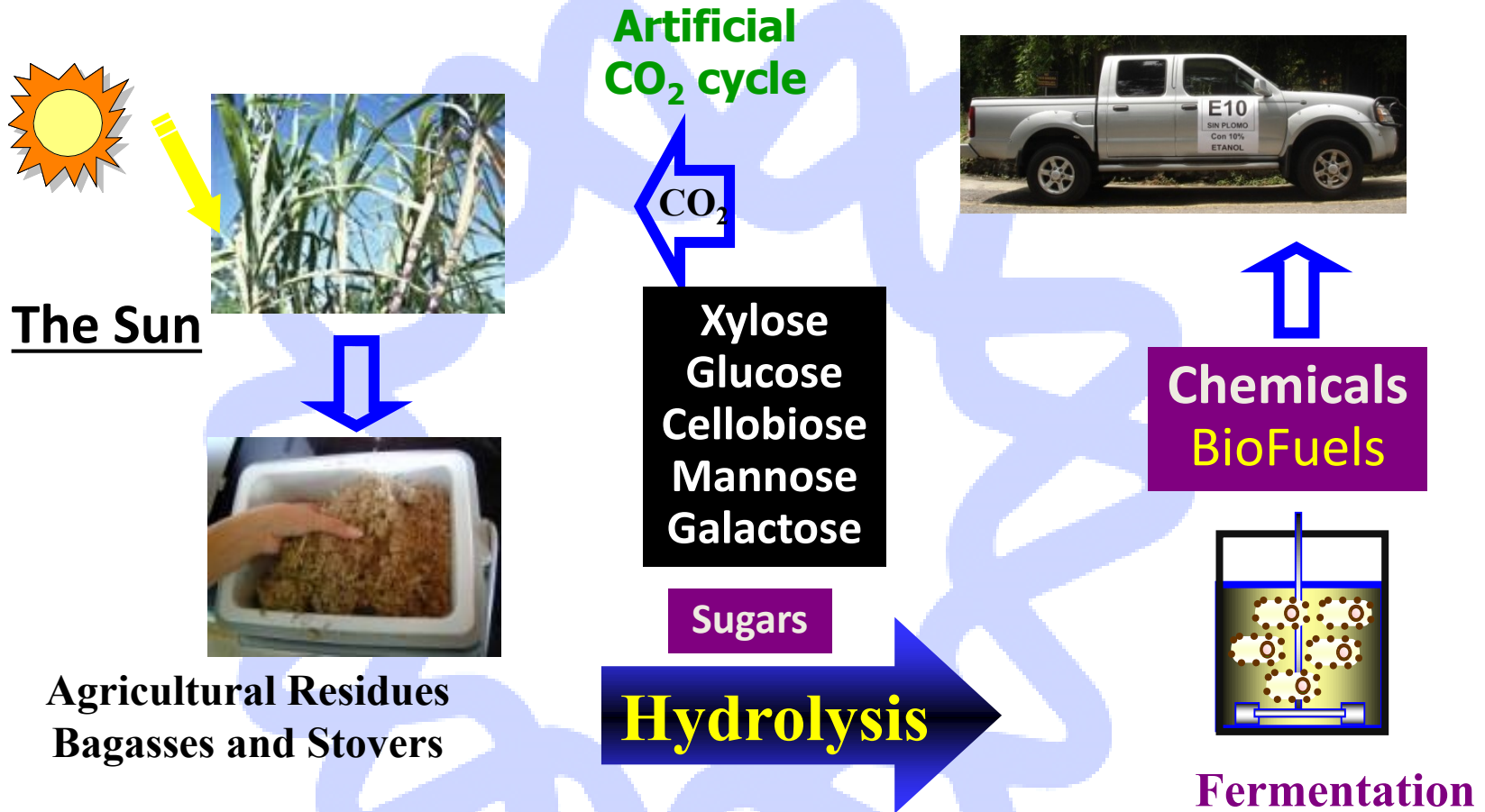
Liquid Bio-fuels
For Transportation

Fuel Ethanol

Biodiesel

Biodegradable
Bioplastics
& Chemicals

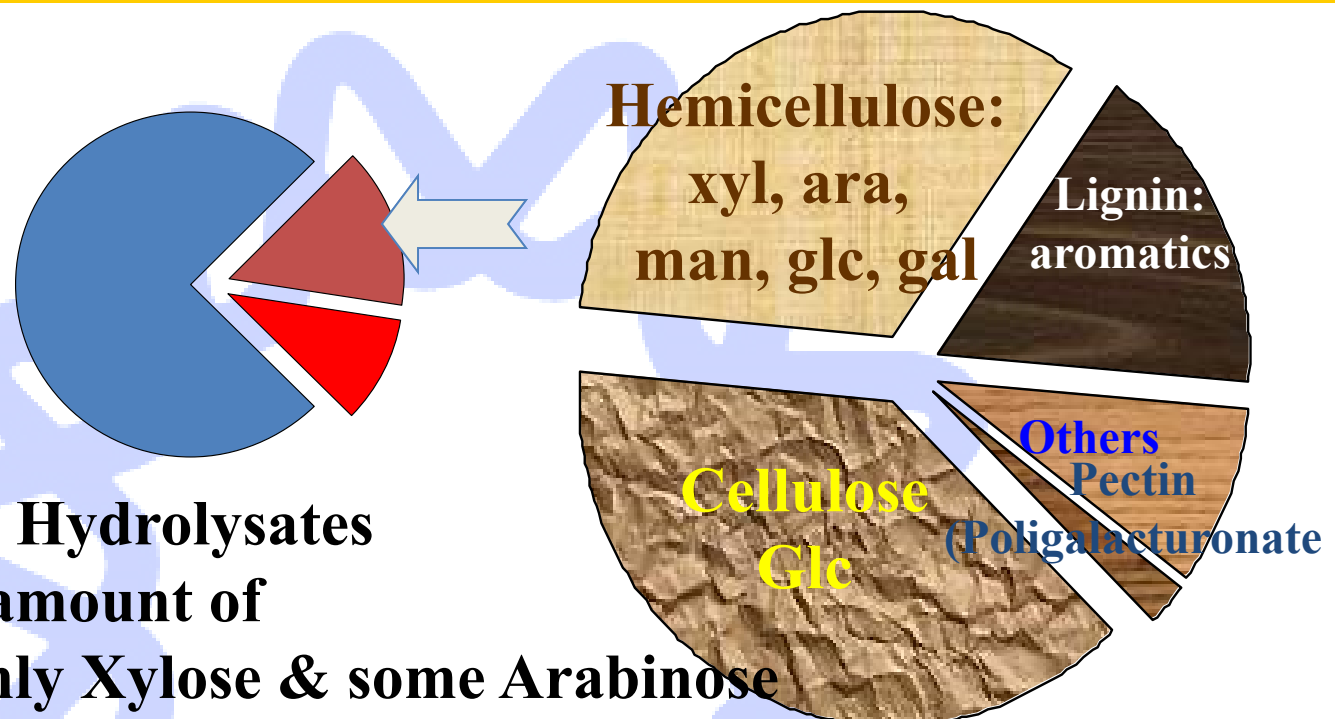
Biorefineries: Biofuels and Chemicals from Lignocellulose



Purpose: Design microorganism and process to transform ALL the SUGARS contained into lignocellulose (cellulose: glucose & hemicellulose: pentoses, hexoses, disaccharides) to biofuels or chemicals with homofermentative strains

Carreón Rodríguez et al., 2009

Generation Ethanol (Agro-Fuels) and (Agro-) Chemicals from Lignocellulose



Lignocellulose Hydrolysates
Contain high amount of
Pentoses, mainly Xylose & some Arabinose
Hexoses, mainly glucose
and Glucuronate, Acetate and Furans

Purpose: Design microorganism and process to transform ALL the SUGARS contained into lignocellulose (cellulose: glucose & hemicellulose: pentoses, hexoses, disaccharides) to ethanol (or other chemicals)



BIO-REFINERÍA

Sol + CO₂ → Biomasa → Combustibles:
Sólidos, Gaseosos y Líquidos

Productos de Fermentación

Bio-Refinería →
Bio-Combustibles

Bio-Plásticos

Bio-Polímeros

Bio-Resinas

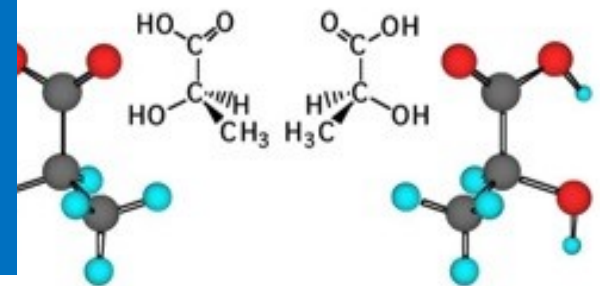
Bio-Químicos



¡~ 1 año!
vs Petróleo
Costos

**Bio-Plásticos
Son 3 R**

BIODEGRADABLE
AMIGABLE CON EL MA
RENOVABLE
H₂O



Martínez 2009



The BioTech. Challenge: Pentoses → Biochemicals

Metabolic Pathway Engineering: XYLOSE

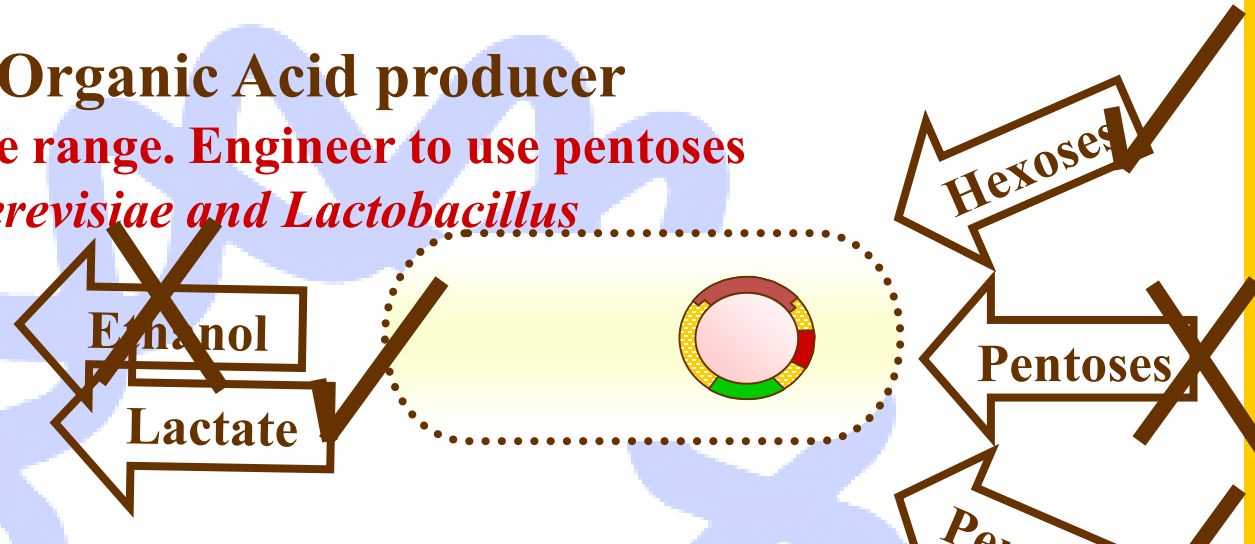
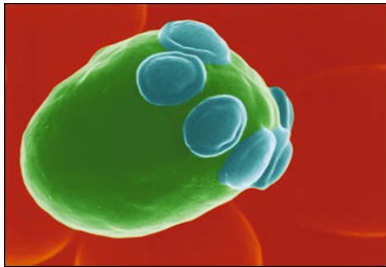


Universidad Nacional Autónoma de México

Instituto de Biotecnología

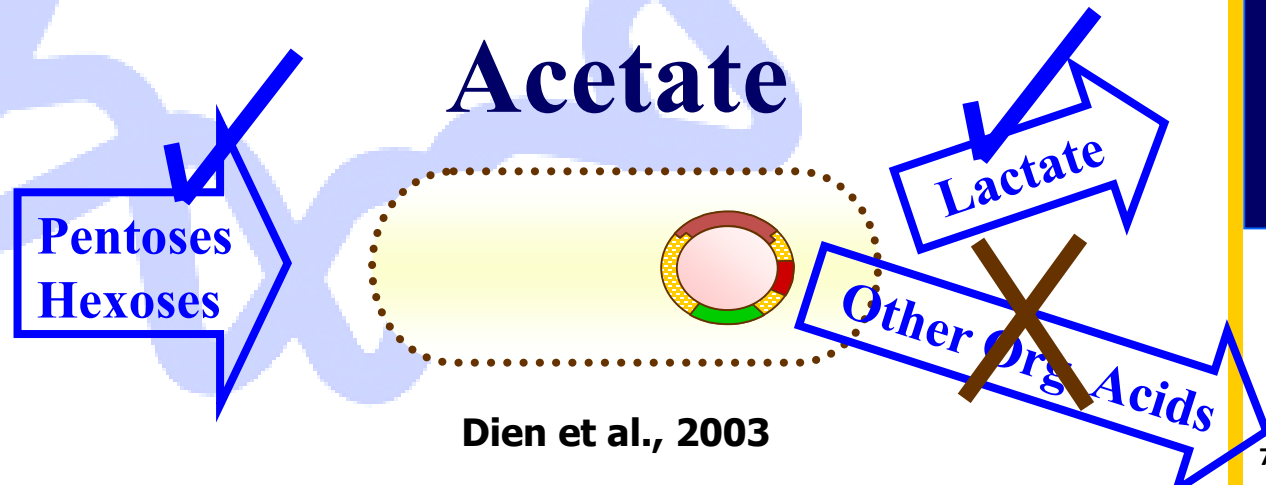
A: Ethanol or Organic Acid producer

Increase substrate range. Engineer to use pentoses
Saccharomyces cerevisiae and *Lactobacillus*



B: NO good Ethanol or Organic Acid producer

Pathway complementation. Engineer to produce only ethanol or lactate, etc.
Escherichia coli



Dien et al., 2003



Who is *Escherichia coli*?

What does *E. coli* do for humans?



E. coli: Bacteria

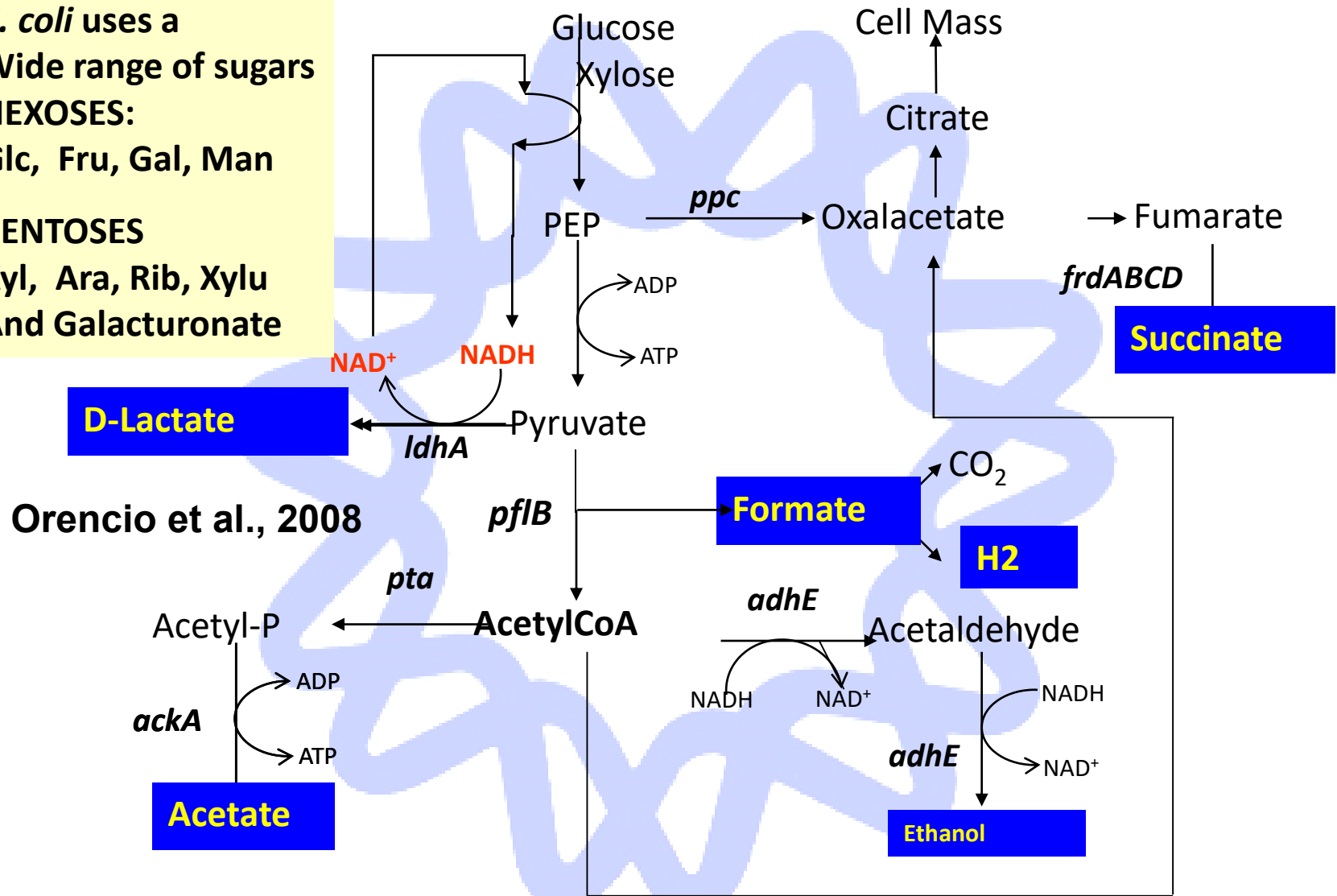
- ❑ Approximately 33% of the therapeutic proteins for human use are currently produced with *E. coli* in industrial fermenters.
- ❑ Human growth hormones; interferons; interleukins; erythropoietin; among others
- ❑ L-phenylalanine, PHB, and 1,3-Propanediol and 1,4-BDO
- ❑ Easy to manipulate & cultivate



Fermentation Products *Escherichia coli*



E. coli uses a
Wide range of sugars
HEXOSES:
Glc, Fru, Gal, Man
PENTOSES
Xyl, Ara, Rib, Xylu
And Galacturonate



Orencio et al., 2008

and make a mix of fermentation products → Homo Fermentative



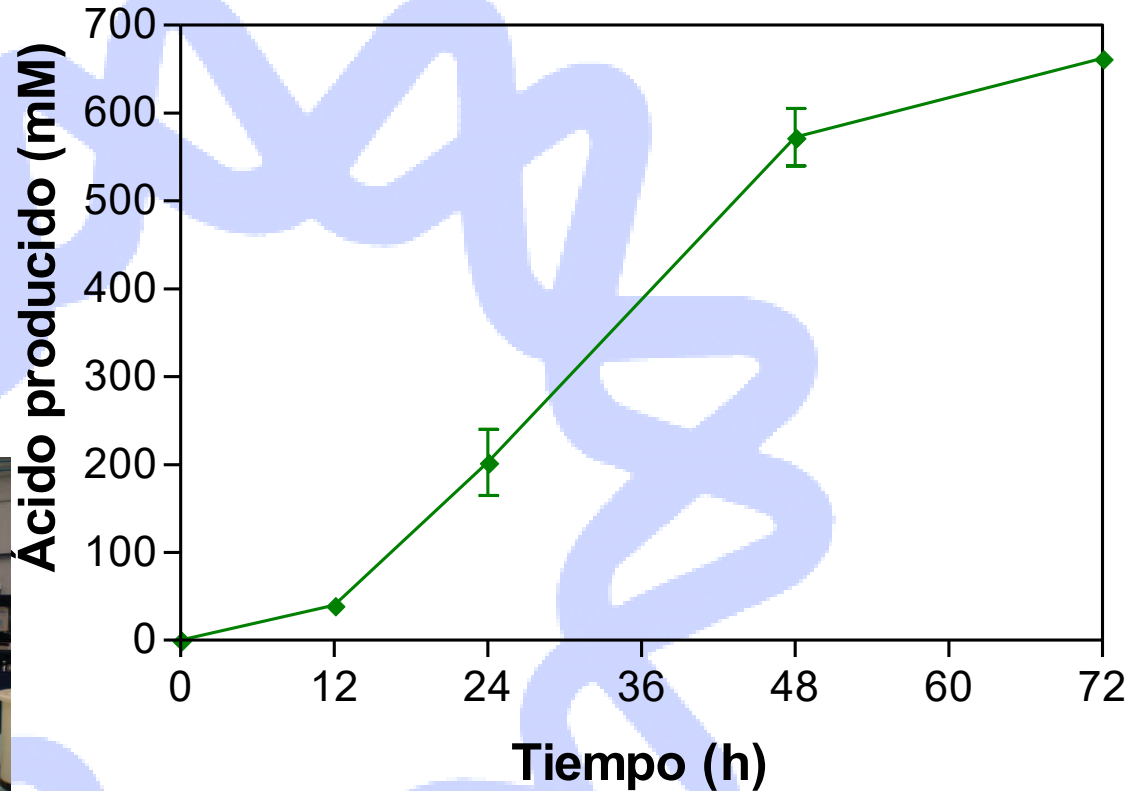
Sugar Cane Bagasse Hemicellulosic Hydrolysate

60 g/L total sugars, acetic acid

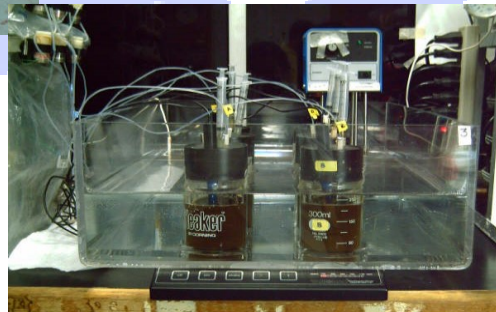
Aprox. 1 g/L Cells



Hydrolysate +
0.9 g/L $(\text{NH}_4)_2\text{HPO}_4$ –
 $\text{NH}_4\text{H}_2\text{PO}_4$
1 mM Betaine
0.1 g/L Citric acid



Utrilla et al., Bioresour Technol. 2017



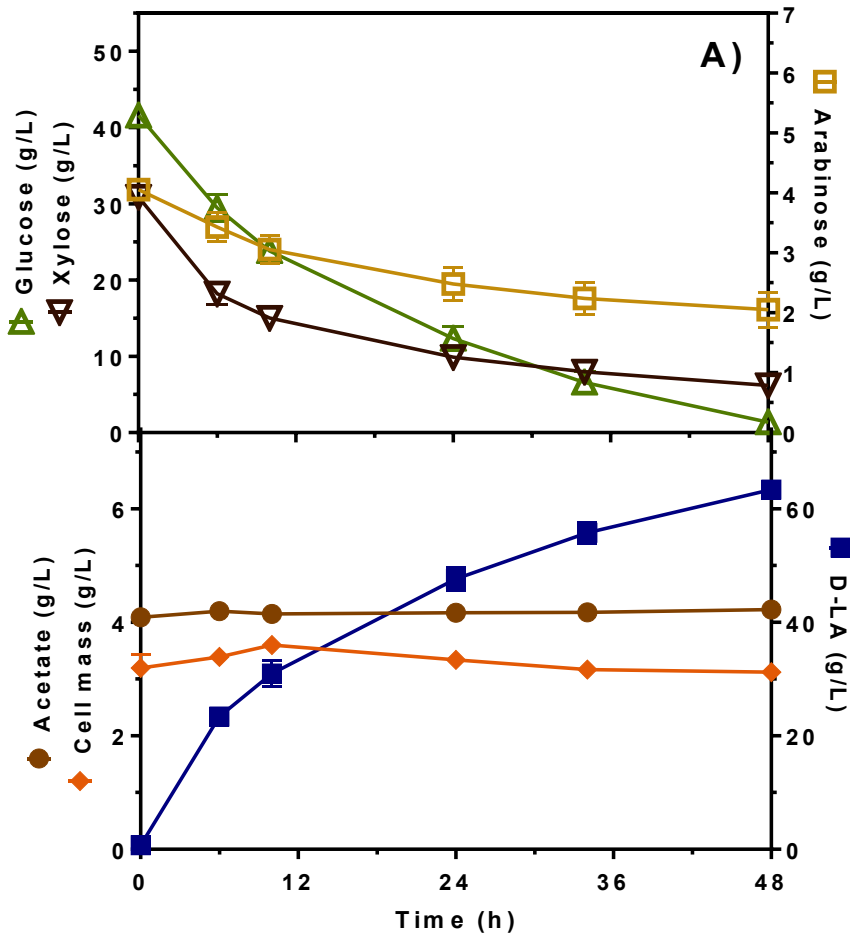


Stover from White Corn

Sequential: Thermochemical Hydrolysis, Enzymatic Saccharification and Fermentation, without detoxification

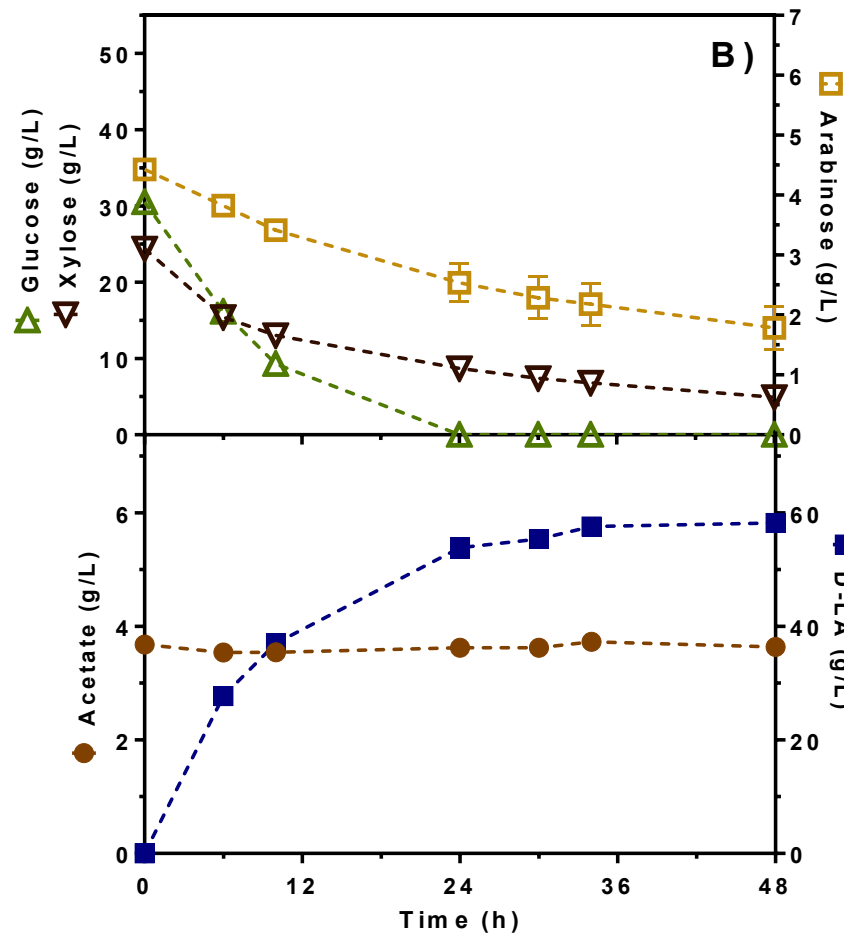


A) Simulated hydrolysate B) Corn Stover hydrolysate



$$Y_{D-LA} (g_{D-LA}/g_{Sugars}) = 0.95 \pm 0.010$$

$$Q_{D-LA} (g_{D-LA}/L h) = 1.32 \pm 0.025$$



$$Y_{D-LA} (g_{D-LA}/g_{Sugars}) = 1.11 \pm 0.064$$

$$Q_{D-LA} (g_{D-LA}/L h) = 1.21 \pm 0.050$$

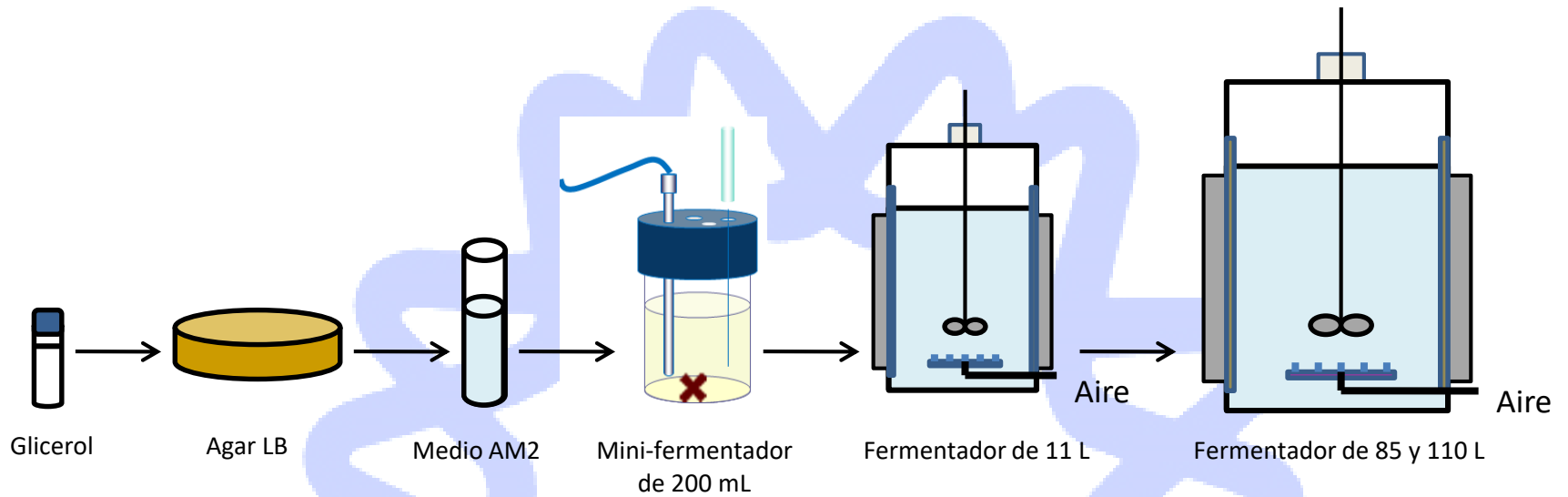
AV03: JU15 Δ poxB, Δ ackA-pta, Δ mgsA
 Simultaneous sugar consumption

Y > 1 !!!

Utrilla et al. Bioresource Technol. 2016



Laboratory Scale-Up: 1, 11, 130 L



Glicerol

Agar LB

Medio AM2

Mini-fermentador
de 200 mL

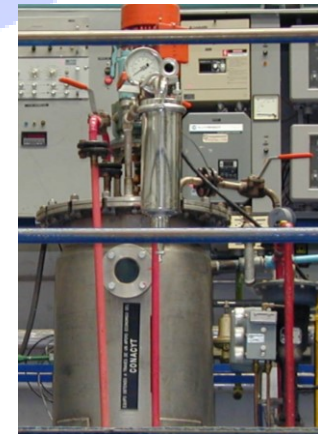
Fermentador de 11 L

Fermentador de 85 y 110 L

Aire

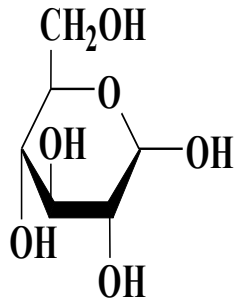
Aire

Sierra et al.,
Submitted.
March 2019

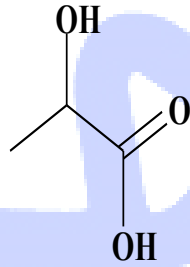




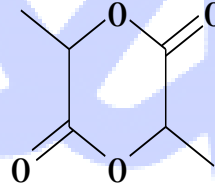
L - Lactato Ópticamente Puro



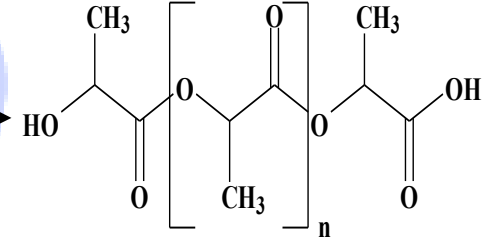
Glucosa



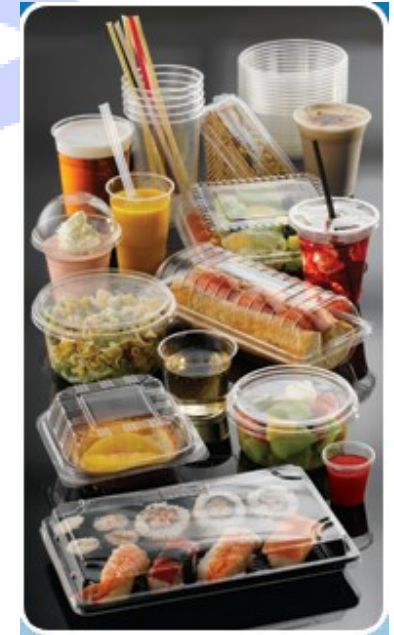
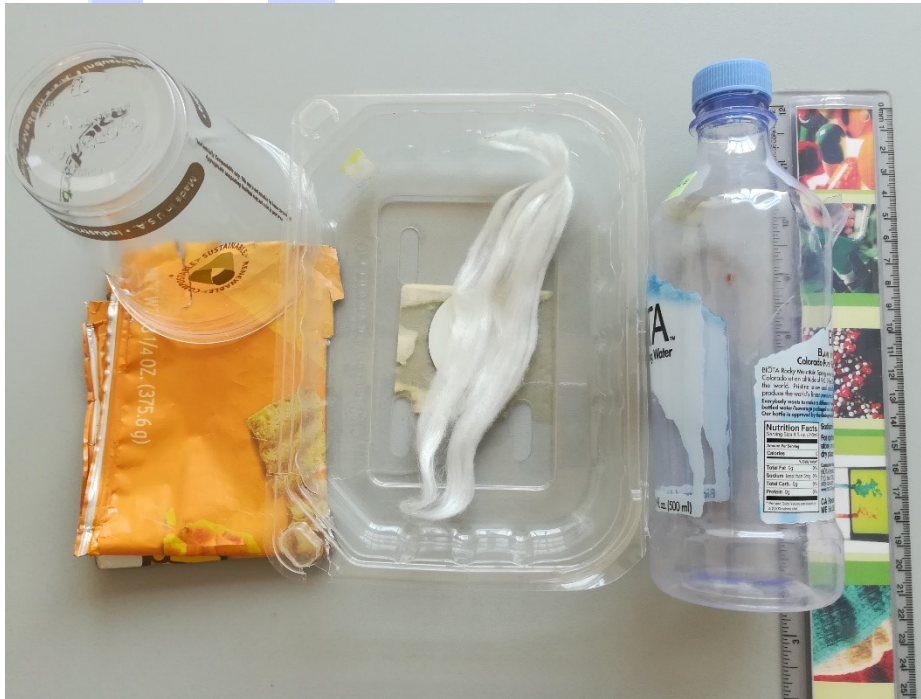
Láctico



iiiiDímero!!!!



iiiiPLLA!!!!

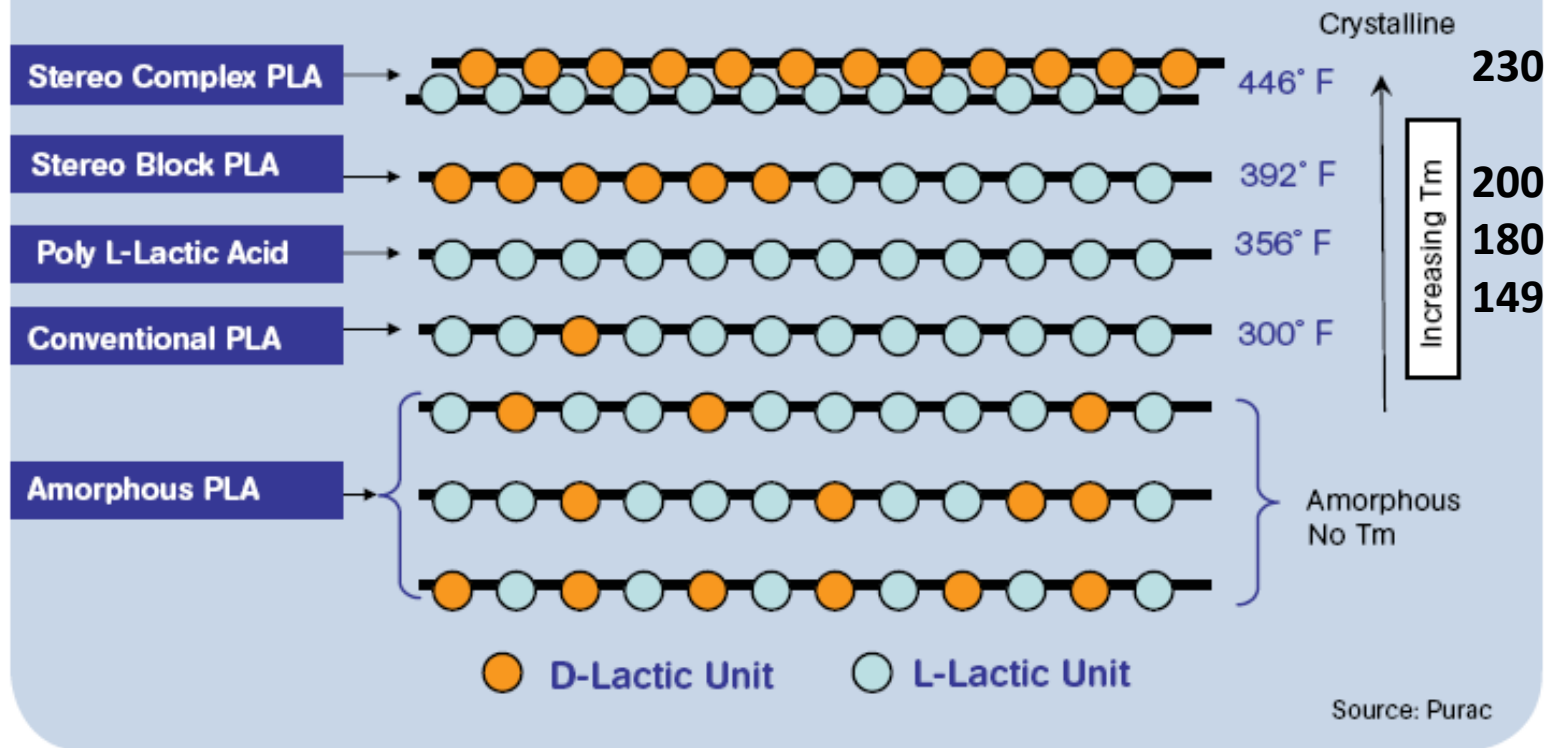




PLA: PLLA sc-PLA



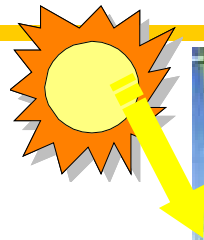
PLA is actually a family of (co-)polymers of D- and L-Lactic units



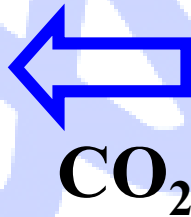
Purac's newly available D-lactide monomer is the "secret" ingredient in some high-heat PLA copolymers in development. Shown here (top to bottom): D/L lactide structures of stereocomplex (sc) PLA, stereo-block-copolymer PLA, poly-L-lactide homopolymer, standard PLA, and amorphous PLA.



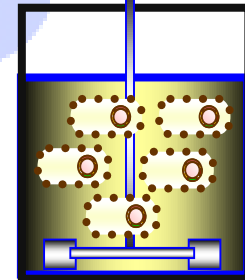
Second Generation Bio-Plastics



Artificial
CO₂ cycle



Lactate



Fermentation

The Sun



Lignocellulose - Biomass
Agricultural Residues
Sugar Cane Bagasse

1 kg of Sugar Yield 1 kg of Lactic Acid
➤ 1 USD / kg; PLLA: > 4 USA dol/kg
Demand 2020 > 1000,000 ton

Xylose,
Cellobiose
Glucose,
etc.
Cellulose,
Hemicellulose

Hydrolysis

Purpose: Design microorganism and process to transform Lignocellulose (cellulose & hemicellulose: pentoses, hexoses, disaccharides) to optically pure lactates (D&L): Biopolymer Precursors



LA production from corn stover with ethanologenic bacteria

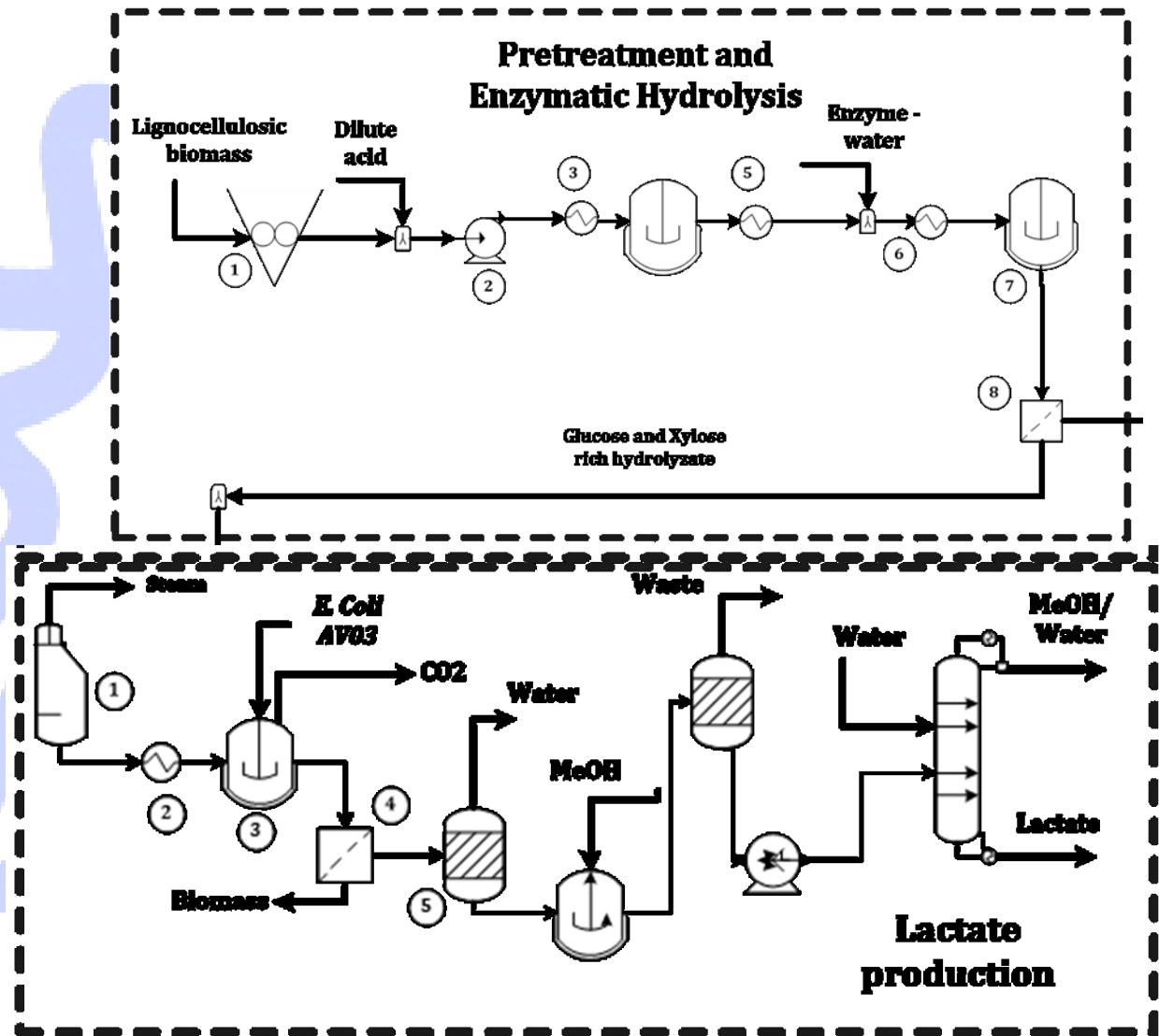


Process Integration
Lab scale: $\sim 520 \text{ kg}_{\text{LA}}/\text{Ton}$





Feedstock: **No wash**
Feedstock: **No dry**
Pretreatment: **No detoxification**
Saccharification: **No separation of C5 and C6 streams**
Fermentation: **All sugars, C5 and C5**
Multiple-Products



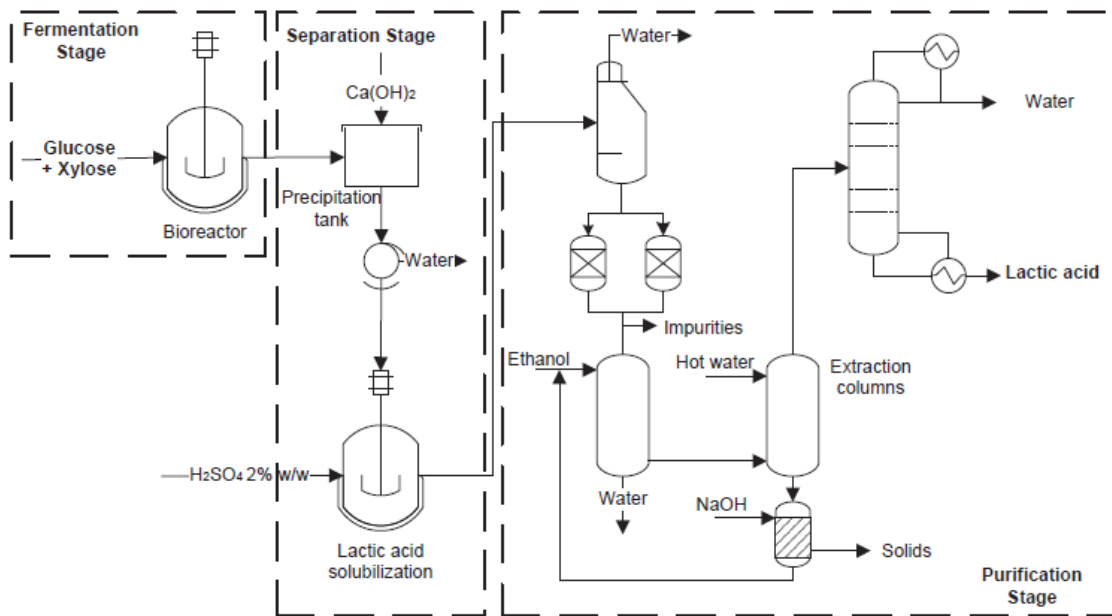


Fig. 1. The lactic acid production process.

Parra, Martinez, Cardona. Biores. Technol. 2019, 273:86-92

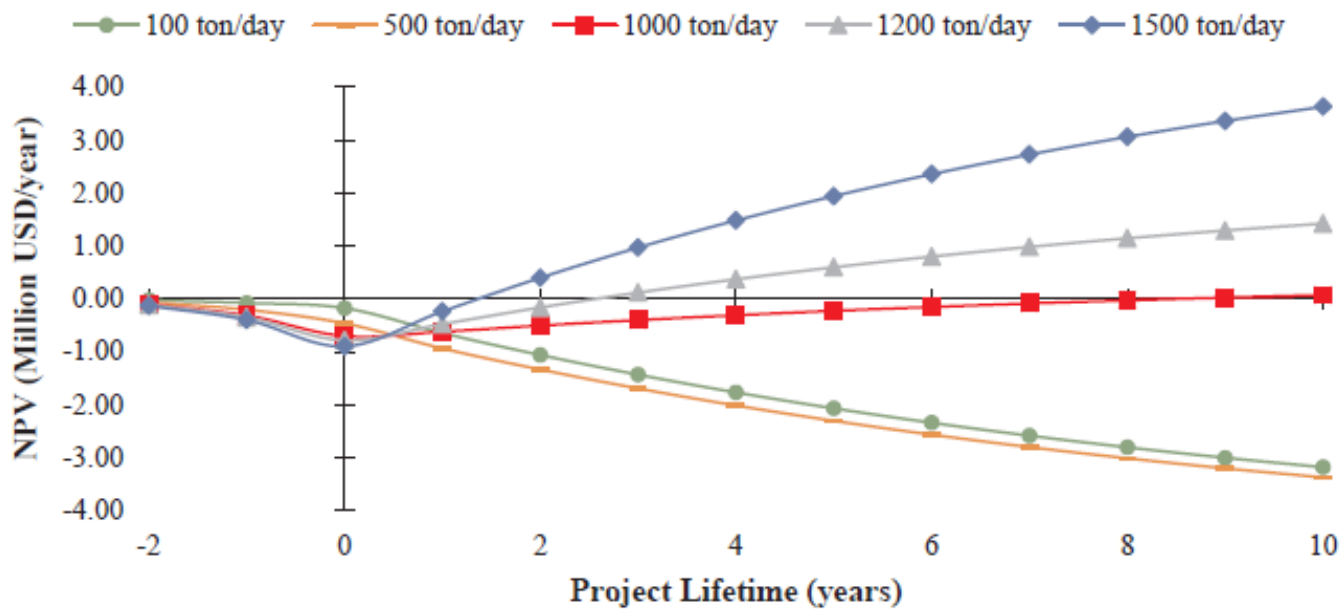


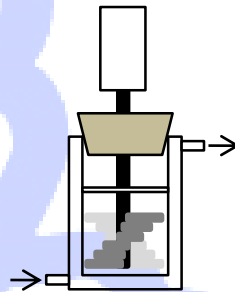
Fig. 4. NPV over project lifetime at different scales.

Stover from White Corn: Sequential: Thermochemical Hydrolysis, Enzymatic Saccharification and Fermentation

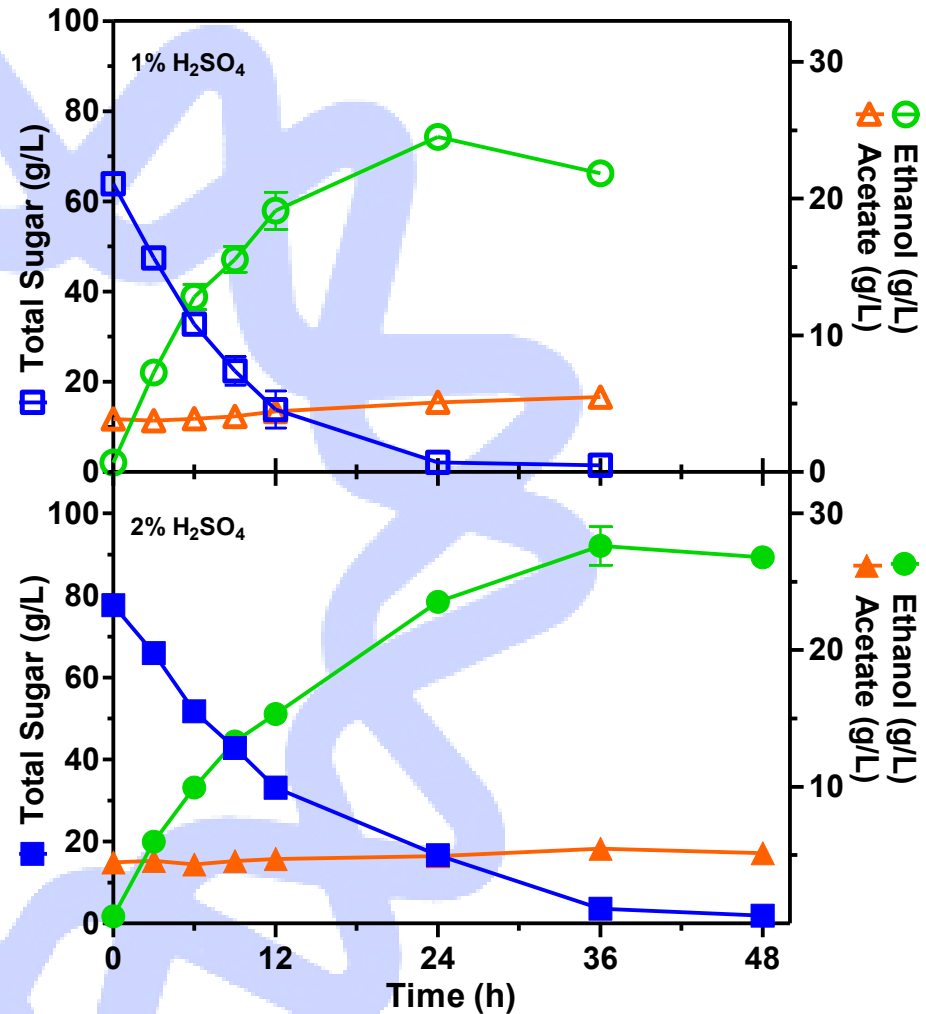
1 kg of Sugar Yields 0.51 kg of EtOH
~ 0.5 USD / L

Non-aerated Cultures with
Ethanologenic *E. coli* MS04, 3.7
g/L, 0.2 L, 37°C, pH 7, 100 rpm.
No salts were added. No detox.

Vargas-Tah et al.,
Bioresource Technol.
2015



Comment
Small Scale Biorefinery: Ethanol



All sugars are fermented to ethanol
by ethanologenic *E. coli* MS04 in 36 h



Bagazo de Agave



Adición de Ácido



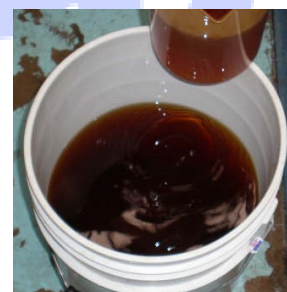
Tratamiento Termoquímico



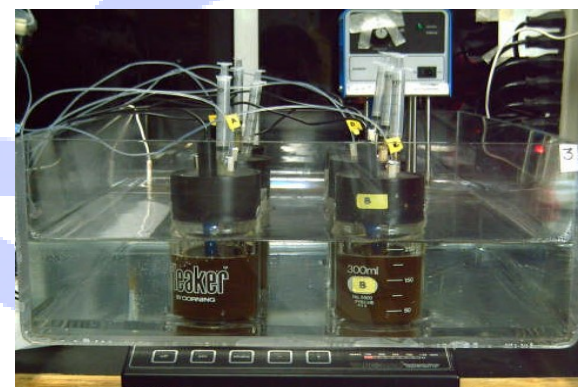
Celulosa Pretratada



Hidrólisis Enzimática



Jarabe de Pentosas



Fermentación



Destilación



Secado



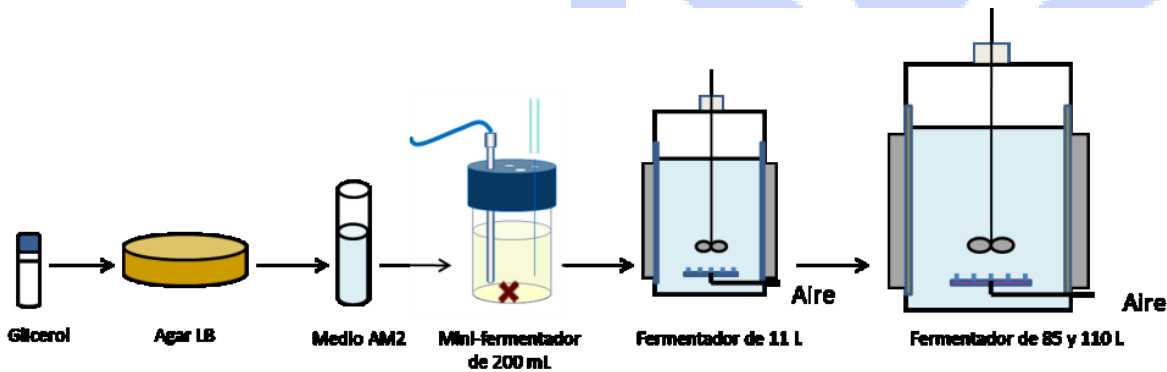
Etanol Carburante

Integración del Proceso en el IBt - UNAM

330 L_{EtOH}/Ton Bagazo de Agave Seco



Lactic acid & Ethanol: Scale-up



$k_L a$ Scale-up

Corn stover hydrolysates

0.2 → 400 L

Yield: > 83%

Productivity

>1 (0.5) g/L/h

Fernández-Sandoval et al. J. Chem Technol Biotechnol. 2017



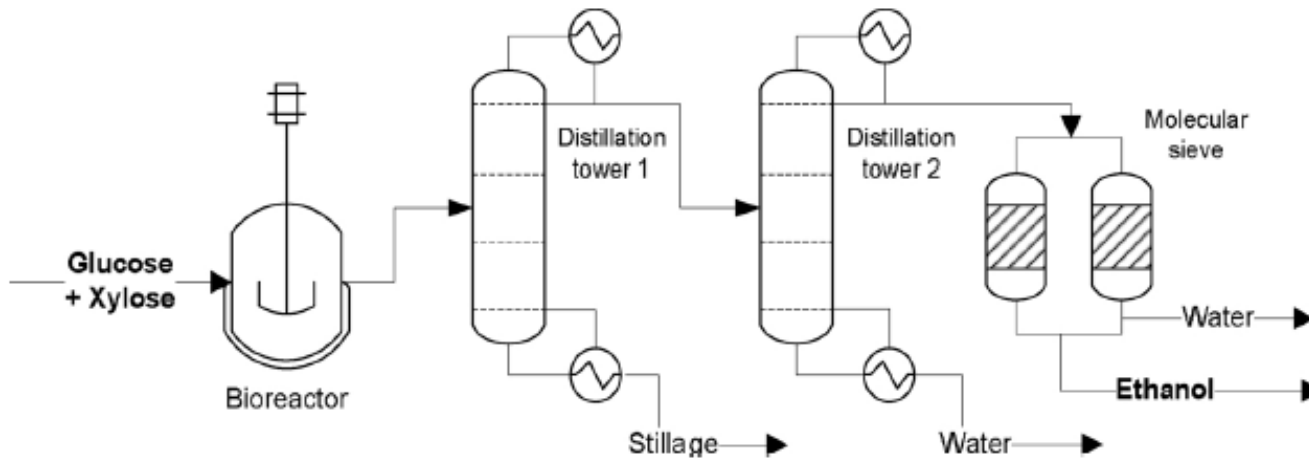


Fig. 1. The production process of ethanol.

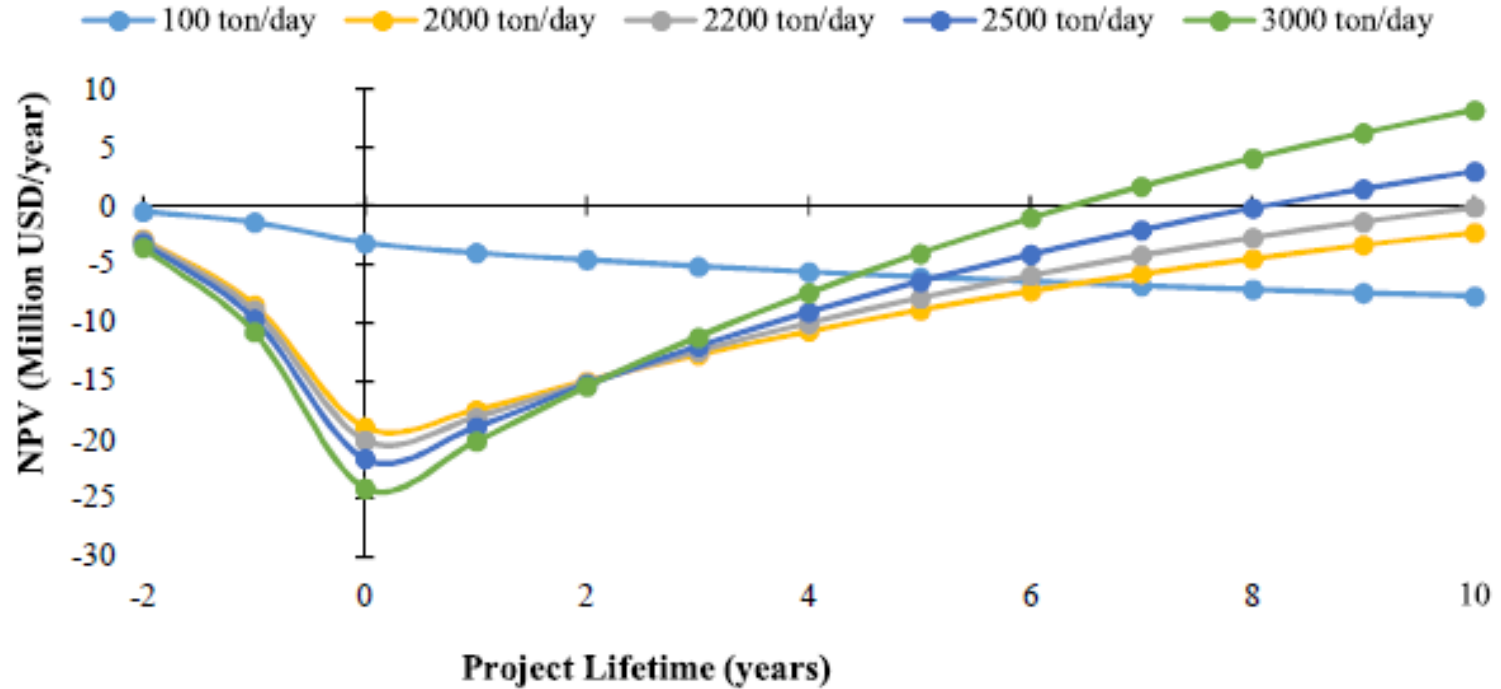


Fig. 7. Net present value of the process at different scales.

Pyruvic acid: Strain JU15 Δ ldhA: MS01

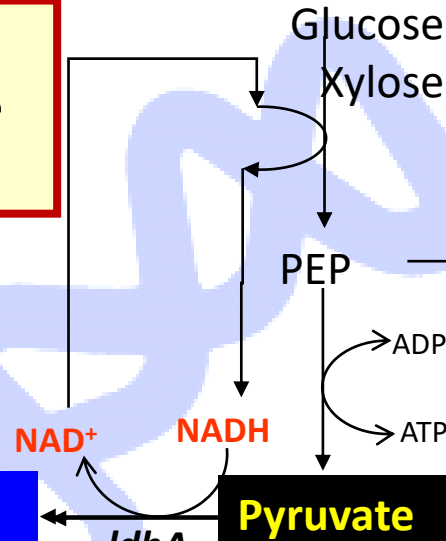


1 kg of Sugar Yields
0.98 kg of Pyruvate
> 1 USD / kg

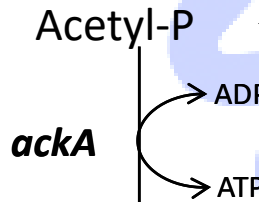
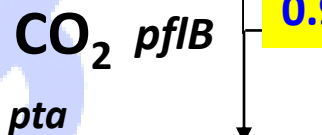
1.00

D-Lactate

L-Lactate



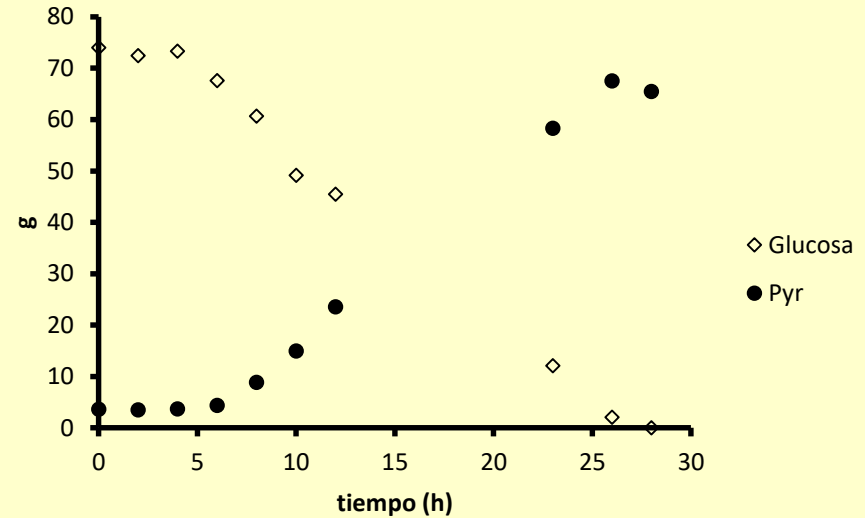
0.98



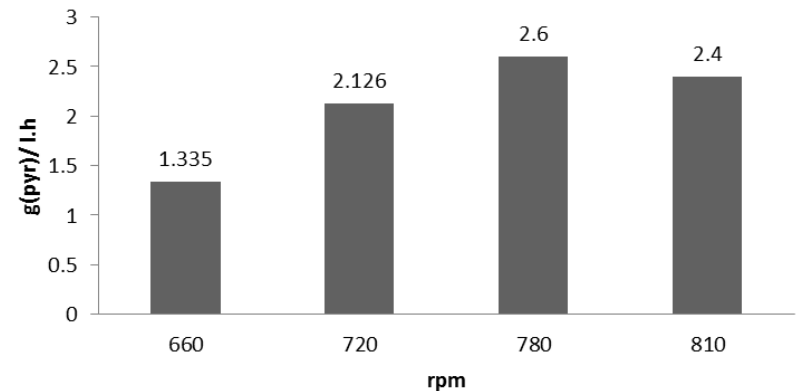
0.65

Acetate

Consumo glucosa/ producción pyr (780)

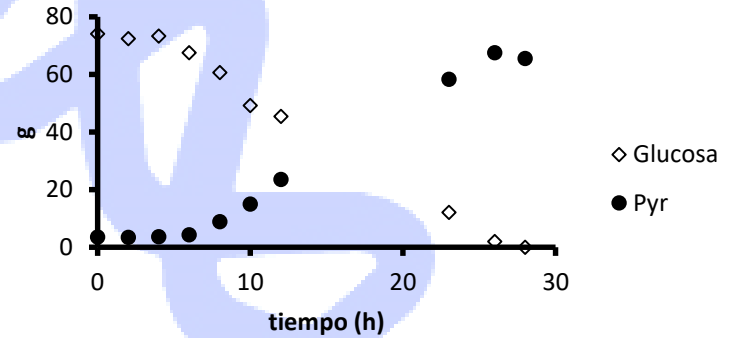


Productividad volumétrica Q_p

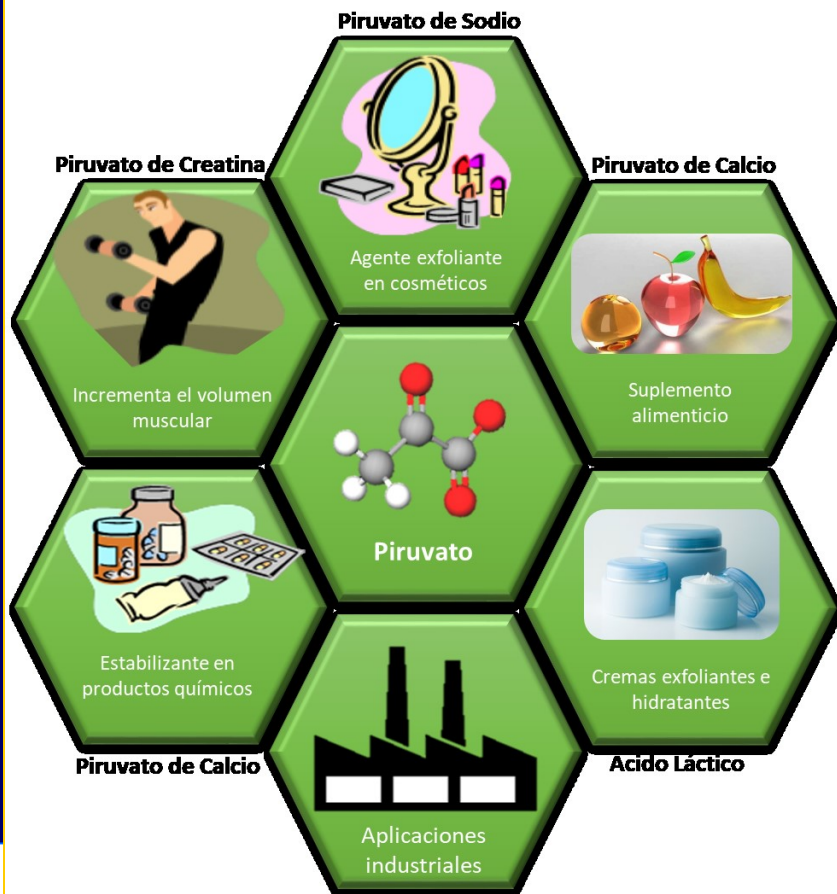
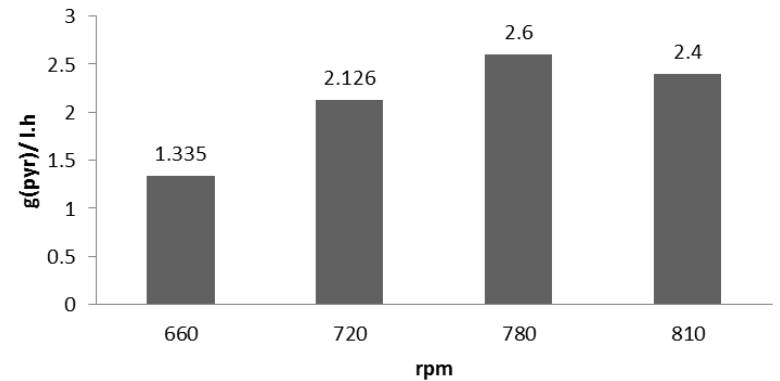


Pyruvic acid. Strain JU15 Δ ldhA

Consumo glucosa/ producción pyr (780)

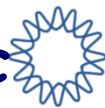


Productividad volumétrica Qp





Succinic acid: Strain JU15 $\Delta IdhA$ *frdA* *P*_{trc} *pck* Δppc



**1 kg of Sugar Yields
1-1.3 kg SA
> 3 USD / kg**

1.00

D-Lactate

L-Lactate

NAD⁺

NADH

CO₂

pflB

pta

Acetyl-P

AcetylCo

ackA

ADP

ATP

Acetate

0.65

Glucose
Xylose

Cell Mass

Citrate

PEP

ppc CO₂

Oxalacetate

→ Fumarate

ADP

Pck → ATP

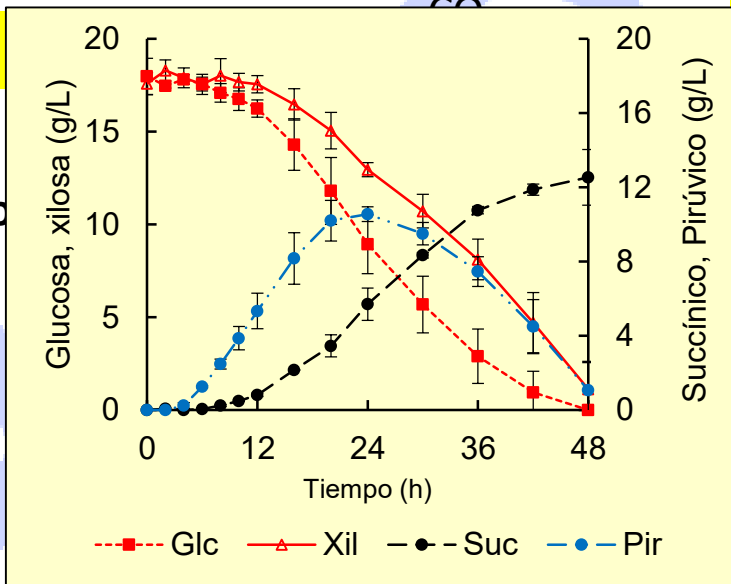
frdABCD

0.51

Succinate

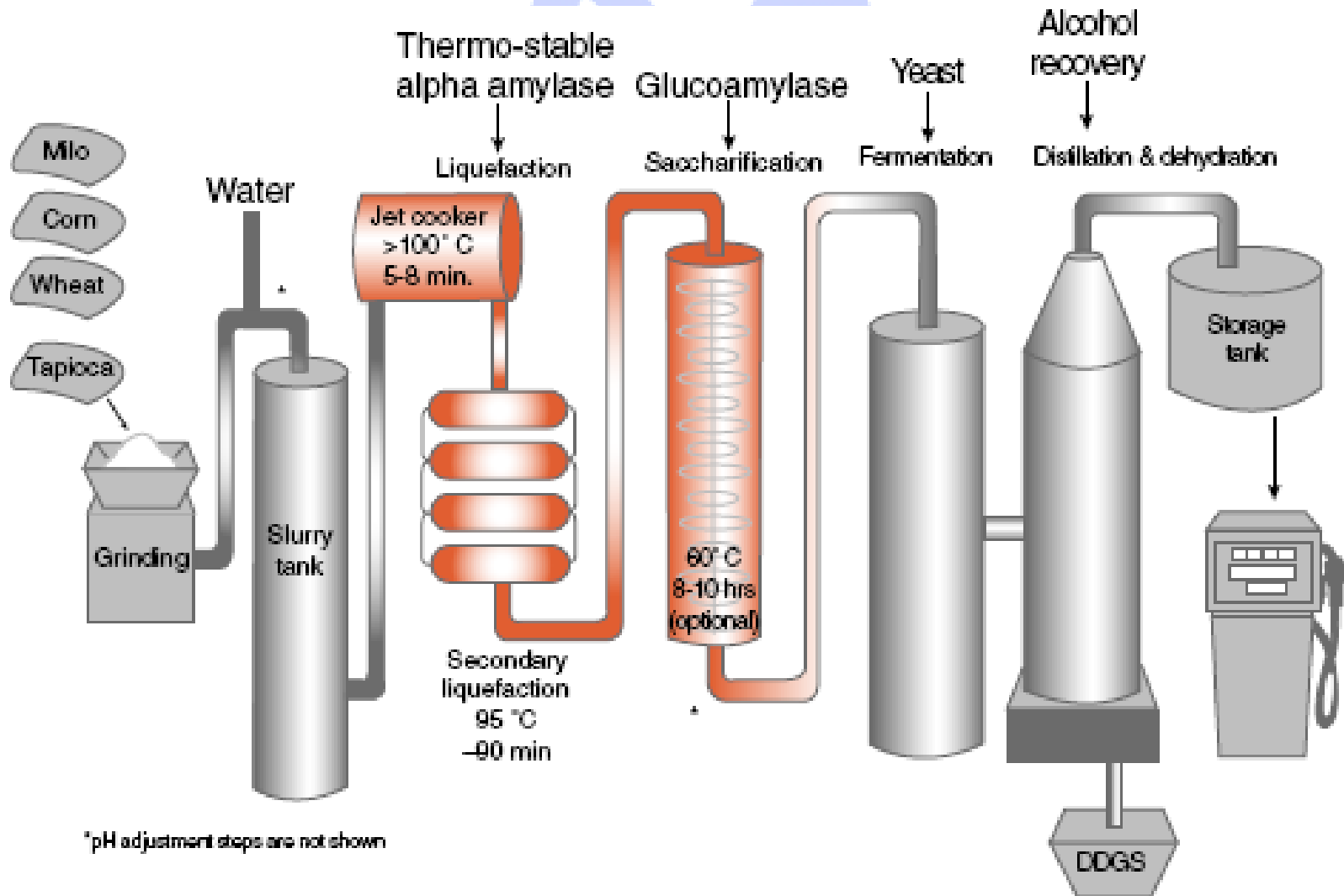
GLUCOSA + XILOSA

**> 1.00 -
1.30**





Proceso maduro para la producción de etanol a partir de granos





Bio-Refinería: Caña de Azúcar

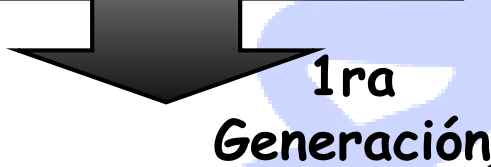




Combustibles Fósiles Necesidad de E. Renovables

Biocombustibles

Combustibles Fósiles
Y Biocombustibles
Actuales



Almidón
Sacarosa
Bio-Etanol

Aceites de Plantas
Bio-Diesel

Lignocelulosa
Bio-Etanol
Bio-Butanol

Oleaginosas no comestibles
Biodiesel
Bioturbosina



CO_2
Algas y
Cianobacterias
H₂ Fotobiológico
Bio-Diesel
Bio-Petróleo
Bio-Turbosina



Biorefinería
Bioplásticos
Biosolventes

Proteínas Alimento
Ácidos grasos
Aceite comestible
Etc.

Biocombustibles – Biorrefinerías
Mediano y Largo Plazo